FIG. 1

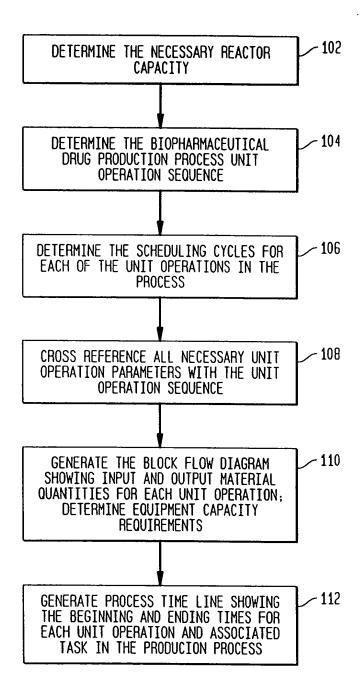
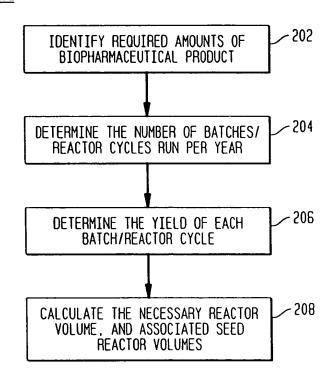


FIG. 2





 $FIG.~~\mathcal{B}$ unti operations LIS

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			OFFSET	豎		324
		PROCESS	UnOp	2		325
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						318
			OFFSET	瓷		316
		BATCH	<u>e</u>	· 名	999992	314
İ		BA	e S	STARIT	ਜਜਜਜਜ ®®®ਜ਼ੁਜ਼	312
			·			350
	CYCLES PER	UnOp	JFFSF1	(FS)		∕ ≋
	נאכו	=				386
MICROBIAL FERMENTATION PROCESS		1		UNIT OPERATION TYPE	INOCULUM PREP FLASK GROWTH SEED FERMENTATION PRODUCTION FERMENTATION PRODUCTION FERMENTATION HEAT EXCHANGE CONT. CENTRIFUGATION/MOLE CELL HARVEST RESUSPEND CELL PASTE HEAT EXCHANGE HEAT EXCHANGE RESUSPENSION/SUBFACTANT CONT. CENTRIFUGATION/PRECIPITATE HARVEST RESUSPENSION/SUBFACTANT CONT. CENTRIFUGATION/PRECIPITATE HARVEST RESUSPENSION/SUBFACTANT CONT. CENTRIFUGATION/PRECIPITATE HARVEST RESUSPENSION/SUBFACTANT CONT. CENTRIFUGATION/PRECIPITATE HARVEST PRODUCT ADSORPTION MPLC ULTRAFIL TRATION/FLOW DIALYSIS PRODUCT ADSORPTION MPLC ULTRAFIL TRATION/FLOW DIALYSIS PRODUCT ADSORPTION MPLC MICROFIL TRATION/FLOW DIALYSIS PRODUCT ADSORPTION MPLC MICROFIL TRATION/DEAD END	
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MICROB			<u>ම</u> දි	<u></u>		- <u>2</u> 2

FIG. 4

CODE UNIT OPERATION TYPE LINITIAL SEEDING CULTURE VESSEL SPLIT CULTURE VESSEL SPLIT CULTURE VESSEL SPLIT CULTURE VESSEL SPLIT STRINGEN FLASK SPLIT STIRRED TANK REACTOR GI HARVEST FRED GZ HARVEST POOL 34 MF/TANGENITAL FLOW 39 PAC/MPLC 39 PAC/MPLC 37 UF/CONCENIRATION 39 PAC/MPLC 37 UF/LOW DIALYSIS 39 PAC/MPLC 35 MF/DEAD END 99 END	1	B 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8
NSC NO	CODE UNIT OPERATION TYPE CULTURE VESSEL SPLIT SULTURE VESSEL SPLIT CULTURE VESSEL SPLIT SULTURE VESSEL SPL	888

FIG. 5

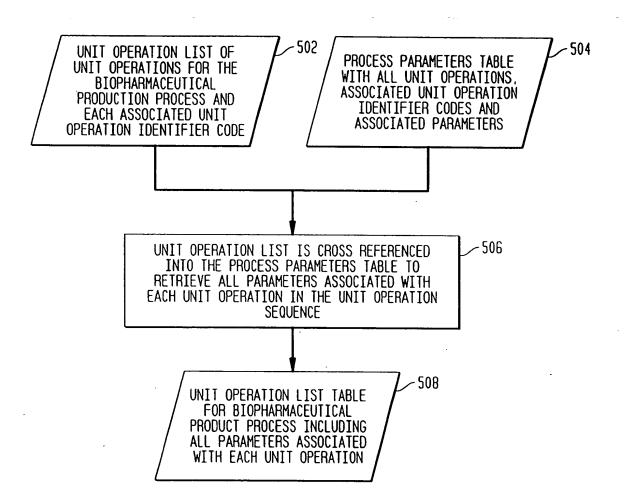


FIG. 6A

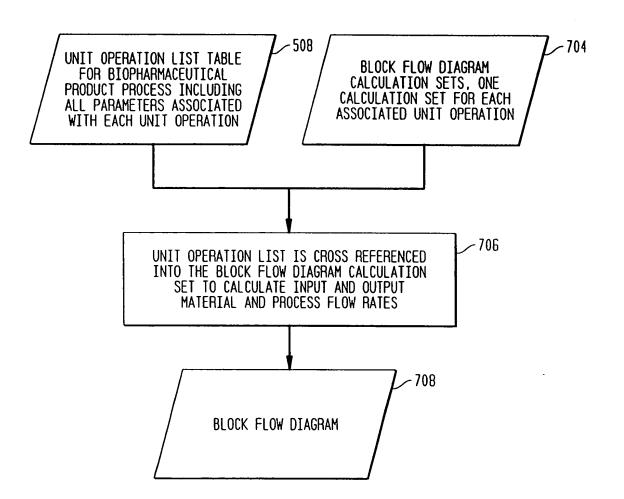
UNIT OPERATION ID CODE	UNIT OPERATION TYPE	PARAMETERS
1	INOCULUM PREP	• OF FLASKS, VOLUME OF FLASKS, TEMPERATURE, AGITATION, DURATION, FINAL OD
2	Flask growth	SCALE UP RATIO, MEDIA VOLUME, TEMPERATURE, AGITATION, DURATION, FINAL OD
3	FERMENTATION SEED	SCALE UP RATIO, FERMENTOR WORKING VOLUME, ANTIFOAM, BASE ACID, GROW TEMPERATURE, AGITATION, SPARGE RATE, BACK PRESSURE, TOTAL DURATION
4	FERMENTATION PRODUCTION	SCALE UP RATIO, GERMENTOR WORKING VOLUME, ANTIFOAM A. ANTIFOAM B. BASE, ACID, GROW TEMPERATURE, AGITATION, SPARGE RATE, BACK PRESSURE, TOTAL DURATION, FINAL OK, DRY CELL MASS, PRODUCT CONCENTRATION, CIP, SIP
5	HEAT EXCHANGE	PROCESS INITIAL & FINAL TEMP; UTILITY INITIAL & FINAL TEMP; PROCESS SPECIFIC HEAT; DESIGN TYPE, STEP RECOVERY OF PRODUCT, STEP RECOVERY OF T.P., TEMPERATURE REGULATION, CIP, SIP
6	BATCH CENTRIFUGATION	SYSTEM VOID VOLUME, RCF. TIME. VOLUME REDUCTION, WASH VOLUME, CLEAN, RINSE
1	RESOLUBLIZATION RESUSPENSION	REAGENT/PRODUCT RATIO, TITRATION SOLUTION, RESOLUBLIZATION, AGITATION, SOLUTION NAME, STEP RECOVERY OF THE PRODUCT, STEP RECOVERY OF T.P., TEMPERATURE REGULATION, CIP, SIP
8	CELL DISRUPTION HIGH PRESS. HOMNOGENIZATION	PRODUCT TERMPERATURE, UNILITY TEMPERATURE, VOID VOLUME, NUMBER OF PASSES, PRESSURE, FLOW RATE, TEMPERATURE INCREASE, WASH, RINSE, STEP RECOVERY OF PRODUCT, STEP RECOVERY OF T.P., TERMPERATURE REGULATION, CIP
9	DILUTE WITH SURFACTANT	REAGENT PRODUCT RATIO, TITRATION SOLUTION, DILUTION TIME, AGITATION, SOLUTION NAME, STEP RECOVERY OF PRODUCT, STEP RECOVERY OF T.P., TEMPERATURE REGULATION, CIP, SIP
10	BATCH CENTRIFUGATION PRECIPITATE HARVEST	SYSTEM VOID VOLUME, RCF. TIME, VOLUME REDUCTION, WASH VOLUME, CLEAN, RINSE, STEP RECOVERY OF PRODUCT, STEP RECOVERY OF T.P., TEMPERATURE REGULATION, CIP, SIP
11	RESUSPEND WITH CHAOTROPE	REAGENT/PRODUCT RATIO, TITRATION SOLUTION, RESOLUBLIZATION, AGITATION, SOLUTION NAME, STEP RECOVERY OF PRODUCT, STEP RECOVERY TO TP, TEMPERATURE REGULATION, CIP, SIP
•		•

FIG. 6B

504

SOLUTION TYPE	TASKS	TASK DURATION
S-101	SETUP, PREINCUBATION, Incubation, Clean up	3, 3, 23, .3, HRS
S-101	SETUP, PREINCURATION, Incubation, Clean UP	1, 1, 23, .3, HRS
S-101, 102, 103, 104, 105	SETUP, PREINCUBATION, FERMENTATION, HARVEST, CIP, SIP, CLEAN UP	1, 1, 21, .5, 1, 1, 3 HRS
S-101, 102 103, 104, 105	SETUP, PREINCUBATION, Fernentation, CIP, SIP, Clean UP	•
	SETUP, TRANSFER, CIP, SIP, CLEAN UP	•
S-106	SETUP, CENTRIFUGATION, WASH, CIP, SIP, CLEANUP	•
S-107	SETUP, DILUTION, AGITATE, CIP, SIP, CLEAN UP	•
S- 10 7	SETUP, LYSIS, CIP, SIP, CLEAN UP	•
S-108	SETUP, DILUTION, AGITATE, CIP, SIP, CLEAN UP	•
S-108	SETUP, CENTRIFUGATION, WASH, CIP, SIP, CLEAN UP	•
S-109	SETUP, FLUSH, PRIME, Concentration, dilution, Wash, Flush, Store, CIP, SIP, Cleanup	•
•	•	•

FIG. 7



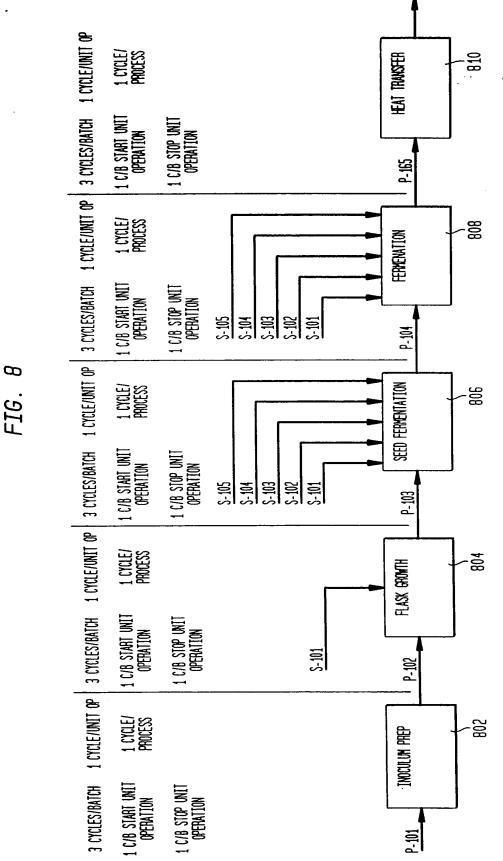


FIG. 9

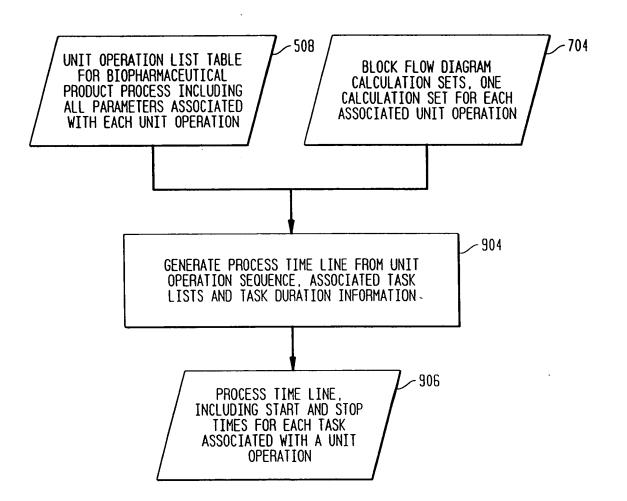


FIG. 10

SAMPLE APPLICATION OF PROCESS DESIGN CYCLES IN PROCESS SCHEDULING

MI

MICROBIAL FERMENTATION PROCESS (SEE UN	IT OPERATION LIST)		.··
		FIRST PROCESS CYCLE	SECOND PROCESS CYCLE
	DURATION	WEEK DAY	WEEK DAY
NOTE: NONE OF THE UNIT OPERATIONS IN T (SEE UNIT OPERATION 8 IN THE MAMMALIA)			
UNIT OPERATIONS 1-6 UNDERGO THREE REPORTED THIS TRANSLATES TO THREE RUNS ON A FEI ASSOCIATED WITH EACH FERMENTOR RUN (U	RMENTOR WITH EACH HARVES VIT OP 4) ARE THE PREVIO	ST (UNIT OP 5 & 6) BEING STORED	FOR POOLING AT UNIT OP 7
1/3 FERMENTATION CYCLES PER BATCI 1 INOCULUM PREP 2 FLASK GROWTH 3 SEED FERMENTATION 4 PRODUCTION FERMENT. 5 HEAT EXCHANGE 6 CENTRIFUGATION 2/3 FERMENTATION CYCLES PER BATC	24 HRS 24 HRS 24 HRS ATION 24 HRS 1 HR 1 HR	1 FRI - SAT 2 SAT - SUN 2 SUN - MON 2 MON - TUE 2 TUE 2 TUE	
1 INOCULUM PREP 2 FLASK GROWTH 3 SEED FERMENTAION 4 PRODUCTION FERMENT 5 HEAT EXCHANGE 6 CENTRIFUGATION	24 HRS 24 HRS 24 HRS ATION 24 HRS 1 HR 1 HR	2 SUN - MON 2 MON - TUE 2 TUE - WED 2 WED - THU 2 THU 2 THU	•
3/3 FERMENTATION CYCLES PER BATC 1 INOCULUM PREP 2 FLASK GROWTH 3 SEED FERMENTAION 4 PRODUCTION FERMENT 5 HEAT EXCHANGE 6 CENTRIFUGATION UNIT OPERATION 7 POOLS THE HARVESTS F	24 HRS 24 HRS 24 HRS ATION 24 HRS 1 HR 1 HR	2 TUE - WED 2 WED - THU 2 THU - FRI 2 FRI - SAT 2 SAT 2 SAT	3 TUE - WED 3 WED - THU 3 THU - FRI 3 FRI - SAT 3 SAT 3 SAT
7 POOL HARVESTS UNIT OPERATION 7 POOLS THE HARVESTS UNIT OPERATIONS 8-9 UNDERGO THREE REF THIS TRANSLATES TO THREE CONSECUTIVE (UNIT OP 8 & 10) AT THE INLET AND THI 1/3 DISRUPTION CYCLES PER BATCH 8 HEAT EXCHANGE	3 HR PETATIVE CYCLES PER BATC PASSES THROUGH CELL DIS E OUTLET OF THE CELL DIS	3 MON H AS SET BEFORE CONTINUING WITH BRUPTOR (UNIT OP 9) WITH ITS AS	4 MON H UNIT OPERATION 11 SOCIATED HEAT EXCHANGERS
9 CELL DISRUPTION 10 HEAT EXCHANGE 2/3 DISRUPTION CYCLES PER BATCH 8 HEAT EXCHANGE 9 CELL DISRUPTION	0.5 HR	3 HON	4 MON
10 HĒAT ĒXCHANGE 3/3 DISRUPTION CYCLES PER BATCH 8 HĒAT EXCHANGE 9 CELL DISRUPTION		3 MON	4 MON
10 HEAT EXCHANGE	0.5 HR	3 KON	4 MON

FIG. 11

SAMPLE APPLICATION OF PROCESS DESIGN CYCLES IN PROCESS SCHEDULING

MICROBIAL FERMENTATION PROCESS (SEE UNIT OPERATION LIST)

MICHORIAL FERMENTATION PRO	NCE22 12EE ANTI ALEM	HIGH CIOH				
			FIRST PROC	ESS CYCLE	SECOND	PROCESS CYCLE
	DUF	ATION	WEEK	DAY	WEEK	DAY
UNIT OPS 11-12 UNDERGO T THIS TRANSLATES TO TWO C SURFACTANT AND RECONCENT 1/2 PRODUCT WASHING	YCLES OF RESUSPENDING RATING THE INSOLUBLE CCYCLES PER BATCH	STHE CELL TYSATE FROM PRODUCT TO A PASTE BY	THE CELL DECENTRIFUGAT	ISKOPIOK IN A MILL)	MON
).5 HR	3 KON			MON
	12. 00 20	1 HR	3 MON		4	NUN
<u>-</u>	G CYCLES PER BATCH	n C 180	2 NOV		4	MON
		0.5 HR	3 HON			MON
12 CENTI	RIFUGATION	1 HR	3 NON	ור ההחפרפפ	9	nun
UNIT OPS 13-22 UNDERGO (ONLY ONE CYCLE PER UN	II OPEKATION EACH TO TH	IE ENU UT I	HE SHORE 22		MON
		0.5 HR	3 MON			MON
		2 HR	3 MON			MON
		2 HR	3 MON			MON
	ID CHRONATOGRAPHY	16 HRS	3 MON	- TUE		MON - TUE
17 LIOU	ID CHRONATOGRAPHY	4 HRS	3 TUE			TUE
18 BUFF	er exchange	2 HRS	3 TUE			TUE
	ID CHRONATOGRAPHY	2 HRS	3 WED			WED
	ER EXCHANGE	2 HRS	3 WE			WED
Ž1 LĪQU	ID CHRONATOGRAPHY	2 HRS	3 WE)		WED
	RATION	2 HRS	3 WEI		4	WED
Et IIII	1817 2411					

Appl. No. To Be Assigned; Filed: HEREWITH
Dkt. No. 1606.0010003; Group Art Unit: TBA
Inventor(s): Peter G. BROWN; Tel: 202/371-2600
Title: System And Method For Simulation And Modeling...

FIG. 12A-1

CALC. A/O ADJ. CALC. A/O ADJ. 3.0 0.0 3.0 HRS 3.0 0.0 3.0 HRS 23.0 0.0 23.0 HRS 1.0 0.0 1.0 HRS 1.0 0.0 23.0 HRS 23.0 0.0 23.0 HRS 1.0 0.0 1.0 HRS

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12A-2	548844 548858			4.38	4.45 4.46 4.54				64.7			_	\sim
	8.54.84.4.8 4.83.33.54.88.4.8			~~	4.45			4.33	4.43			0.56	6)
FIG.	105.0 106.0 108.0				106.0 107.0 109.0				106.4 107.4 107.9				8)
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	82.5 83.0			104.5				105.0				14.5 15.5	رو
•	21.0 mm 21.0 mm 1.0 mm 2.0 mm 2.0 mm 2.0 mm 2.0 mm 2.0 mm 3.0 mm	27.0 HRS		0.5 HRS 1.0 HRS	2.1.5 2.1.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3	5.0 HPS		1.0 表	1.0.3 1.0.3	3.85 HRS		1.0 HBS	
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·	21.000.0	27.0		0.50	2:0:0	5.0		888	5283	3.85		1.0	(3
•	4 A PRODUCTION FEMENTATION SET UP PREINCUBATION FEMENTATION CIP SIP CLEAN UP		5 A HEAT EXCHANGE		CIP SIP CLEAN UP		6 A CONT. CENT./SOLIDS		CIP SIP CLEAN UP	SUBTOTAL	1 B INOCULUM PREP	SET UP PREINCUBATION	7)
	**************************************	~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~~		~ ~ ~	423			4.2.8.6				 	(,

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Inventor(s): Peter G. BROWN; Tel: 202/371-2600
Title: System And Method For Simulation And Modeling...

FIG. 12B-

CAL DE	NO ON ON	14-1				ABS. DAYS		OB/03/96	START - DATE TIME 06/03/96 08:00 AM	PINISH			CALCULATIONS	SNOI
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25.0		25.0 HRS		61.5										
			_											
	0.00		61.5	2 2		2.53	2.52	96/50/90	3333	M 06/05/96 12:30 F OF 106/05/96 11:30 F OF 106/05/96 10:30 F OF 10	98.99	Z Z Z		
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4 B PRODUCTION FERMENTATION												,	····	
——— <u>—</u>	1.0000 1.000	1.0 HS 2.1.0 HS 3.0 HS	83.0	104.0		3.4.38	3.45	96/90/90 96/90/90	883	AM 06/06/96 10:00 AM 06/06/96 11:00 AM 06/07/96 08:00 AM	6 10:00 6 11:00 6 08:00	444		

FIG. 12B-2

														
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CIP SIP CLEAN UP	SUBTOTAL	5 B HEAT EXCHANGE	SET UP TRANSFER	CIP SIP CLEAN UP	SUBTOTAL	6 B CONT. CENT./SOLIDS	SET UP CENTRIFUGATION	MASH	SIP CLEAN UP	SUBTOTAL	1 C INOCULUM PREP	SET UP PRETNCHRATTON	INCUBATION CLEAN UP	SUBTOTAL
888	88	8	388	288	55	8	353	<u>e</u>	255	55	<u> </u>	3#2	四当	#5

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Inventor(s): Peter G. BROWN; Tel: 202/371-2600
Title: System And Method For Simulation And Modeling...

FIG. 12C-1

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FIG. 12C-2

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FIG. 12D-:

PROCESS TIME LINE CALC. AID ADJ. PREP EXCL. COMPL. START EN DATE TIME DATE DATA DATE DATA DATE DATE DATE DATA DATA DATA DATA DATA DATA DATA DATA DATA DATA DATA DATA DATA DATA DATA	LPM = 0.30 HBS		
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252 128 128 128 128 128 128 128 128 128 12	TRANSFER CIP SIP CLEAN UP		8 B HEAT EXCHANGE

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FIG. 12D-2

					····	,					_			 -	
0.30 HRS			0.68 HRS				0.30 HRS					0.30 HRS			
]						u					**			
3.7 LPM			1.6 LPM				3.8 LPM					3.7 LPM			
97 S LB			86.5 UB				g 0.69					90.5 LB			
3333			E E E	E E E			E E E	5 E S	5			2 E	是 3	E &	
<u> </u>			25:25	25.55		<u> </u>	22:5	225	? }			8:3 8:8	2:5	95:2	
5 06/07/96 12:52 PH 06/07/96 01:00 PH 06/07/96 01:00 PH 06/07/96 01:00 PH 06/07/96 01:10 PH 06/07/96 01:00 P			06/07/96 06/07/96	06/0//96 01:51 06/07/96 01:51 06/07/96 01:51			1 PM 06/07/96 01:51 F	8//0/98 06/07/98	06/10/du			06/07/96 02:09 06/07/96 02:27	06/07/96	06/07/36 06/07/36	
12:52 PM 01:10 PM 01:10 PM 01:10 PM			01:10 91:15 FF	21:51 21:51 21:51 21:51 21:51			01:21 PH 01:51 PH	25:03 25:03 24:03 24:03	UZ:03 FM			22:03 PF 22:03 PF	22:27 PM	04:27 PP	
36/0/36 06/07/36 06/07/36			96/0/90	8/0/98 8/0/98 8/0/98			06/07/96 01:21 06/07/96 01:51 0	06/0/36 06/07/36	96/0/90			36//0/90	96/0/98	06/07/36 06/07/96	
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109.2 109.2 109.2				5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5				999	7.01				111.5	112.5 113.5	
109.2	109.2		109.9		109.9		110.2		6 97	110.2 	L	110.5			110.5
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0.30	0.3		0.0	000	20		0.50	0.0	0.0			3.8	10.1		3.3
TRANSFER CIP SIP CI FAN UP	1	9 B HOMMOGENIZATION			SUBTOTAL	10 B HEAT EXCHANGE		SIP		SUBTOTAL	8 C HEAT EXCHANGE			SIP CLEAN UP	
8888		£ 83	355	2	3 25	3 25	<u> </u>	<u> </u>	8	<u> </u>	28	388	<u> </u>	<u> </u>	<u> </u>

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FIG. 12E-1

	Page	S II	PROCESS TIME LINE													
	E E	OURATION (H	33.)	图. 1	TIME SCALE (HRS)		ABS. DAYS	475	START		FINISH					
OPERATION	CALC. A/D	,	€.	뫒	ESEC.	COMPL.	START	END	DATE	TIME	DATE	当		CALCULATIONS	SJAC S	
					15.5				96/60/90	06/03/96 08:00 AM						
9 C HOMMOGENIZATION							-									
SET UP	9.6	0.0	0.0 HSS	110.5	=======================================		8.8	8.8	06/07/96 02:27 06/07/96 02:27	02:27 PH 02:27 PH	M 06/07/96 02:27 06/07/96 03:07	02:27 PM 03:07 PM	9) S:99	1.6 LPM	••	0.68 HRS
		000	1.0 元 元 元			112.1	<u>a</u>	4.67	36/10/90 06/10/90	03:07 P	96/0/90 H	04:07 05:07 PE				
CLEAN UP	1.0	0.0	1.0 HRS			11.1	4.71	4.76	96/10/90	05:07 P	M 06/07/98	06:07 PP				
SUBTOTAL	3.7		3.7 HRS		111.1											
10 C HEAT EXCHANGE																
SET UP	0.0	0.0	0.0 景	111.1			3.5	E3.	36/0/30	03:07 P	H 06/07/96	03:07 PM		9		יטיי
IKANSI-ER CIP	90.7	5 O	365]	112.4	3.25	£ 88.	96/0/98 98/0/98	03:07 P 25:09	36/0/90 H	04:25 PP 13:25	93.0	3.0 LFA	**	SE 95.0
SIP CLEAN UP	51	0.0	5.0.1 表表	<u>-</u>	•	113.4	4.68	4.73	06/07/96 04:25 P 06/07/96 05:25 P	04:25 P 05:25 P	5 PM 06/07/96 05:25 F 5 PM 06/07/96 06:25 F	05:25 PM 06:25 PM				
SUBTOTAL	3.3		3.3 HBS		111.4											
11 A RESOLUBLIZATION																
SET UP	1.0		1.0 語	108.9	9		64.7	35.	36/0/98	11:52 A	96/20/90	12:52 PM	מו ט טר	. 20		our ou
ULLUI 10N Agitate	0.5 .5	3.0.	3.5 € € € € 5.0		25. 25. 26. 26. 26. 26. 26. 26. 26. 26. 26. 26		¥.35.	£ 85.	06/07/96 01:22 F	4:22 01:22 P	PH 06/07/96 01:52 F	25.10 1.52 PR	2.08.3 2.08.3 3.	0.3 LTR		0.50 EEE 05.0
	0.0		2.0 E E	-		8 8 8 8	2 2	\$ \$ \$	86/0/38 86/0/38	01:52 P	96//0/90	25:52 25:53 25:53 26:53	_	 		
CLEAN UP	0.0		0.0			109.9	4.58	8	96/0/90	01:52 P	96/0/90	01:52 PM				
SUBTOTAL	2.0		2.0 HBS		109.9											

FIG. 12E-2

	M = 0.50 HRS M = 0.10 HRS M = 0.25 HRS		0.50 HPS 0.50 HPS		LPM = 0.50 HSS LPM = 0.10 HSS LPM = 0.25 HSS		
	8 9.2 LPM 8 0.5 LPM 19 0.5 LPM		Man 6.9		9.2 U 9.2 U 9.5 U 9.5 U 9.5 U	·	
	275.9 3.0 8.0		200 200 200 200 200 200 200 200 200 200		275.9 3.0 8.0	-	
_	796 01:52 796 02:22 796 02:28 796 02:28 796 02:28		786 02:38 786 02:38 786 04:13 786 04:13	8	796 03:13 796 03:43 796 03:49 796 03:04 796 05:04		
	PH 06/07/ PH 06/07/ PH 06/07/ PH 06/07/ PH 06/07/		28 PK 06/07/ 28 PK 06/07/ 13 PK 06/07/ 13 PK 06/07/	<u>æ</u>	3 PM 06/07/96 (3 PM 06/07/96 (9 PM 06/07/96 (4 PM 0		
	06/07/96 12:52 06/07/96 01:52 06/07/96 02:22 06/07/96 02:28 06/07/96 02:28		06/07/36 02:2 06/07/36 02:2 06/07/36 02:5 06/07/36 03:1 06/07/36 04:1	36 35 35	06/07/96 02:13 06/07/96 03:13 06/07/96 03:43 06/07/96 03:49 06/07/96 04:04		
	4.58 4.60 4.60 4.60 4.60 4.60		4.63 4.63 4.63 4.63	4.76	4.65 4.66 4.66 4.71 4.71		
, 	4.54 4.58 4.60 110.5 4.60 110.5 4.60 110.5 4.60		4.60 4.60 4.62 4.63 112.2 4.63 113.2 4.63	_	4.59 112.1 4.66 113.1 4.67 113.1 4.67		_
	110.4	110.5	111.2	111.2	7.111	111.8	
_	109.9		110.5	10.10	111		
_	0.0 #\$S #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$S #\$ 0.0 #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$ 0.0 #\$S #\$ 0.0 #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$ 0.0 #\$S #\$ 0.0 #\$ 0.0 #\$S #\$ 0.0 #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #\$S #\$ 0.0 #		0.0 0.3 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3.5 3	3.8	0.1 HS 0.1 HS 0.1 HS 0.1 HS 0.5 HS 0.5 HS		
_	0.0000	1.6	0.0000.0000.00000.000000000000000000000		0.5000000000000000000000000000000000000	-	
_	264 12 A CONT. CENT/SOLIDS 265 SET UP 267 CENTRIFUGATION 268 CIP 270 SIP 271 CIFAN IP		11 B RESOLUBLIZATION SET UP OILUTION AGITATE CIP		284 12 8 CONT. CENT/SOLIDS 285 SET UP 287 CENTRIFUGATION 289 CIP 290 SIP 21 CIFAN IP		SCALE OF CONTRACT AND TATTOM

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-IG. 12F-1

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		CALCULATIONS									æ.		
			Ì	2.0 LPM			二分子	<u> </u>	当当地		MX FB		1/9/1
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				80.7 LB	1				999	1			22
		1		60.7		ł	25.50	### ## ## ##	2.0.25 2.0.25				33.2 3.2.2
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	E IN	불		96/80/90 96/80/90 96/80/90 96/80/90			96/80/90 96/80/90	88/98 98/98	888 868	96/80/90 96/80/90 96/80/90			AM 06/08/36 AM 06/08/36 AM 06/08/36
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Dkt. No. 1606.0010003; Group Art Unit: TBA
Inventor(s): Peter G. BROWN; Tel: 202/371-2600
Title: System And Method For Simulation And Modeling...

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	OPFRATTON	CALC. A/D	100		皇	EXEC. COMPL. START END	G.	START	8	DATE	<u> </u>	DATE	邕		CALCUL	CALCULATIONS	
						15.5					06/03/96 08:00 AM						
445	S CIFAN IP	1 0 0 0	1	1.0 表			144.9	8.9	6.04	96/00/90	11:54 PI	144.9 6.00 6.04 06/08/96 11:54 PH 06/09/96 12:54 AM	12:54 AM				
7 2 3		2.1	1	2.1 憲		143.6									Æ	EE EE	0.91 LPM
7 7	22 A STERILE FILTRATION		+														0.09 SF
	419 420 SET UP 421 FILTRATION	0.5		0.5 HRS 0.5 HRS	152.6	144.1		£.89.5	6.8	96/00/90	08:05 A	36/09/38	06:36 AM 12:06 AM	2.2 [8	06/09/96 08:06 AM 06/09/96 06:36 AM 06/09/96 11:36 PM 06/09/96 12:06 AM 2.2 L@ 50.0 L/SF/Hr or 0.07 LPM	-/III or	0.07 LP
22	22 STORAGE 33 CIP	0.00		S.S.S.S.S.S.S.S.S.S.S.S.S.S.S.S.S.S.S.			144.6		200	95/50/90 95/50/90 95/50/90	255 255 355 355 355 355 355 355 355 355	# # # # # # # # # # # # # # # # # # #	3.55 3.85 3.85 5.85 5.85 5.85 5.85 5.85				
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22	ł	1.5		1.5 HRS		144.1				,					¥	EE XE	0.07 LPM
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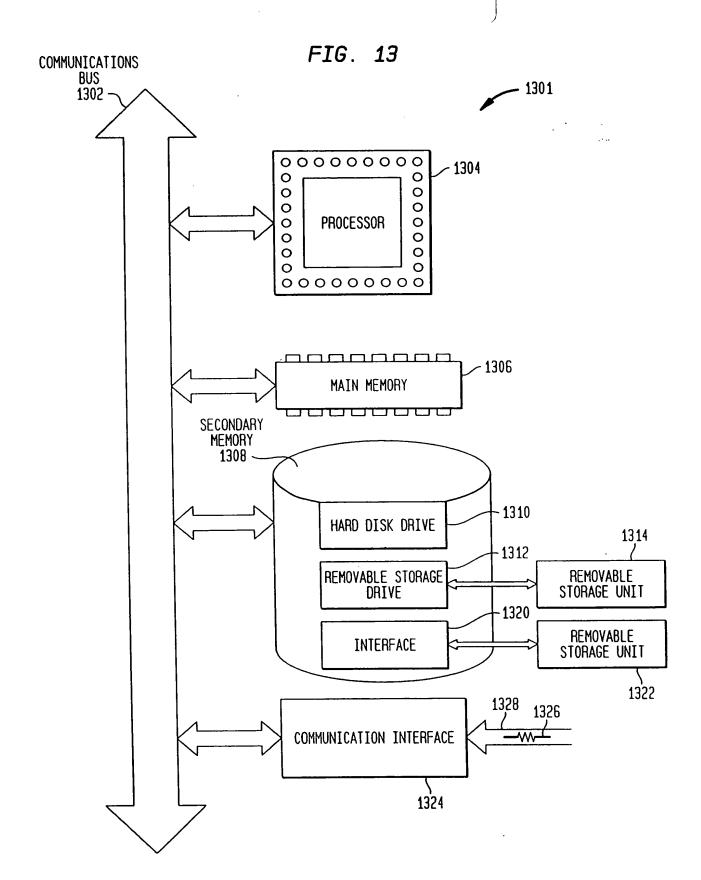


FIG. 14A

		, 10. 1.			
		24045752		ROUP 1	
_	UNIT OPERATION TYPE	PARAMETER	SOLN.		
Ti	INNOCULUM PREP	NUMBER OF FLASKS MEDIA VOLUME/FLASK		2 0.25	LITERS
12	FLASK GROWTH	SCALE UP RATIO Media volume/flask		10 1.25	FOLD L
T3	FERMENTATION Production	SCALE UP RATIO FERMENTOR WORKING VOLUME ANTIFOAN A ANTIFOAN B BASE ACID	S-101 S-102 S-103 S-104 S-105	500 1 1 5	FOLD LITERS MI/L MI/L MI/L MI/L
14	INITIAL SEEDING	NUMBER OF AMPULES VOLUME PER AMPULE STARTING CELL DENSITY AMPULE SPLIT RATIO CULTURE VESSEL TYPE FEED VOLUME		300,000 1 ROLL. BOT. 100	MI CELLS/MI VESSELS/AMPULE MI
15	CULTURE VESSEL SPLIT	VESSEL SPLIT RATIO NEW VESSEL TYPE FEED VOLUNE SERUM CONTENT			MI Fetal boyine serum
16	SPINNER FLASK SEEDING	FLASK FEED VOLUME VESSEL/FLASK RATIO UCARRIER DENSITY MUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES		0.1 5 2	LITERS L. CELLS/L FLASK Gn/LITER FBS
17	BIOSYNTHESIS BIOREACTOR PREPARATION (STIRRED TANK REACTOR)	REACTOR FEED VOLUME SPINNER/REACTOR RATIO UCARRIER DENSITY NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES		500 8.3 5 2 1	Gm/LITER
18	BIOSYNTHESIS BIOREACTOR PREPARATION (HOLLOW FIBER REACTOR)	REACTOR FEED VOLUME NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES SERUM CONTENT			
19	BIOSYNTHESIS BIOREACTOR PREPARATION (FLUIDIZED BED REACTOR)	REACTOR FEED VOLUME UCARRIER DENSITY NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES SERUM CONTENT	6		LITERS Gøs/L
T	O INITIAL SEEDING	NUMBER OF AMPULES VOLUME PER AMPULE STARTING CELL DENSITY AMPULE SPLIT RATIO			2 2 HI 0 CELLS/MI 1 YESSELS/AMPULE

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Title: System And Method For Simulation And Modeling...

. FIG. 14B

	GROUP 2		6	ROUP 3	
PARAMETER	SOLN.		PARAMETER	SOLN.	
TEMPERATURE AGITATION DURATION		37 C 200 RPH 18 HOURS	FINAL OD		12
TEMPERATURE AGITATION DURATION		37 C 200 HOURS 16 RPM	FINAL OD		12
GROWTH TEMPERATURE AGITATION Sparge rate Back pressure Total Duration		37 HOURS 1 HP/100L 1.5 YVM 5 PSIG 21 HRS	FINAL OD DRY CELL MASS PRODUCT CONCENTRATION CIP		9.96 Gas TDCM/L 0.3 Gas PRODUCT/L Y
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE		2.0% FETAL BOVINE SERUM 1 FEED PER VESSEL PER 2 Days 2 Days	AMPLIFICATION FACTOR		100%
FEED RATE Days to confluence		1 FEED PER VESSEL PER 2 DAYS 2 DAYS	AMPLIFICATION FACTOR		100%
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE		2.0% FETAL BOYINE SERUM 1 FEED PER VESSEL PER 2 DAYS 2 DAYS	AMPLIFICATION FACTOR		100%
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE SERUM FREE MEDIA WASHES		2.0% FETAL BOVINE SERUM 1 FEED PER VESSEL PER 2 DAYS 10 DAYS 2	PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.		2500% Mg PROD/L 0.125 Mg TP/MI
NUMBER OF REACTORS FEED RATE DAYS TO CONFLUENCE		1 FEED PER VESSEL PER 1 DAYS 10 DAYS	HARVEST VOLUME PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.		500% LITERS 25 Mg PROD/L 0.125 Mg TP/MI
NUMBER OF REACTORS FEED RATE DAYS TO CONFLUENCE		1 1 FEED PER VESSEL PER 1 DAYS 10 DAYS	PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.		2500% Mg PROD/L 0.125 Mg TP/HI
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE		2.0% FETAL BOVINE SERUM 1 FEED PER VESSEL PER 2 DAYS 2 DAYS	AMPLIFICATION FACTOR		100%

FIG. 15A

	UNIT OPERATION TYPE	PARAMETER	SOLN.	GROUP 1
	UNIT OFENATION TIFE		JULN.	
		CULTURE VESSEL TYPE FEED VOLUME		ROLL. BOT. 100 Mi
T11	CULTURE VESSEL SPLIT	VESSEL SPLIT RATIO NEW VESSEL TYPE FEED VOLUME SERUM CONTENT		RB 100 MI 2.0% Fetal Boyine Serum
112	SPINNER FLASK SPLIT	FLASK FEED VOLUME VESSEL/FLASK RATIO UCAPRIER DENSITY NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES		4 LITERS 0.1 L CELLS/L FLASK 5 Gm/LITER 2 1
T13	BIOSYNTHESIS BIOREACTOR PREPARATION (STIRRED TANK REACTOR)	REACTOR FEED VOLUME SPINNER/REACTOR RATIO UCARRIER DENSITY NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES		500 LITERS 8.3 5 Gm/LITER 2 1 2
T14	BIOSYNTHESIS BIOREACTOR PREPARATION (FLUIDIZED BED REACTOR)	REACTOR FEED VOLUME UCARRIER DENSITY NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES SERUM CONTENT		LITERS GmS/L
T15	INITIAL COUPLING	FLASK FEED VOLUME VESSEL/FLASK RATIO UCARRIER DENSITY NUMBER OF PBS VASHES NUMBER OF MEDIA VASHES NO. OF MEDIA/SERUM VASHES		4 LITERS 0.1 L CELLS/L FLASK 5 Gm/LITER 2 1 2 FBS
T 16	ADDITIONAL COUPLING	REACTOR FEED VOLUME SPINNER/REACTOR RATIO UCARRIER DENSITY NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES		500 LITERS B.3 5 Ga/LITER 2 1
T 17	PEPTIDE CLEAVAGE	REACTOR FEED VOLUME NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES SERUM CONTENT		100 LITERS 2 2 2 2 2 2.0% FETAL BOYINE SERUM
T 18	TISSUE THAWING	CRUDE PRODUCT YEILD ENVIRONMENTAL TEMPERATURE THAN DURATION		25 Ga CRUDE PROD./Kg TISSUE 25 C 16 Hours
	HOMOGENIZATION LIQUID THAVING	CRUDE PRODUCT YEILD LIQUID/SOLID RATIO HOMMOGENIZATION TEMP. HOMMOGENIZER TYPE ENERGY INPUT DURATION		25 Gn CRUDE PROD./Kg TISSUE 10 L SOLUTION/KG TISSUE 4 C RS 200 HP/100L/HR 4 HOURS

FIG. 15B

GROUP 2 GROUP 3					
PARAMETER	SOLN.		PARAMETER	SOLN.	
PBS WASHES TRYPSIN WASH		200 MI 100 MI			٠
FEED RATE DAYS TO CONFLUENCE PBS WASHES TRYPSIN WASH		1 FEED PER VESSEL PER 2 DAYS 2 DAYS 200 MI 100 MI	AMPLIFICATION FACTOR	100%	
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE		2.0% FETAL BOVINE SERUM 1 FEED PER VESSEL PER 2 DAYS 2 DAYS	AMPLIFICATION FACTOR	100%	
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE SERUM FREE MEDIA WASHES		2.0% FETAL BOVINE SERUM 1 FEED PER VESSEL PER 2 Days 10 Days 2	PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.	2500% 0 . 125	Mg PROD/L Mg TP/MI
NUMBER OF REACTORS FEED RATE DAYS TO CONFLUENCE		1 1 FEED PER VESSEL PER 1 DAYS 10 DAYS	PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.	2500% 0 . 125	Mg PROD/L Mg TP/MI
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE		2.0% FETAL BOVINE SERUM 1 FEED PER VESSEL PER 2 DAYS 2 DAYS	AMPLIFICATION FACTOR	100%	
SERUM CONTENT FEED RATE DAYS TO CONFLUENCE SERUM FREE MEDIA WASHES		2.0% FETAL BOYINE SERUM 1 FEED PER VESSEL PER 2 DAYS 10 DAYS 2	PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.	2500% 0.125	Mg PROD/L Mg TP/MI
NUMBER OF REACTORS FEED RATE DAYS TO CONFLUENCE		1 1 FEED PER VESSEL PER 1 DAYS 10 DAYS	HARVEST VOLUME PRODUCT CONCENTRATION TOTAL PROTEIN CONCEN.		LITERS Mg PROD/L Mg TP/MI
CONTAMINANT PROTEIN CONC.		100 Ga/L	TEMPERATURE REGULATION CIP SIP	YYY	
CONTAMINANT PROTEIN CONC.		100 Ga/L	TEMPERATURE REGULATION CIP SIP	YYY	
	-		AMPLIFICATION FACTOR	100%	

FIG. 16A

	•	110. 1	GROUP 1
	UNIT OPERATION TYPE	PARAMETER	SOLN.
			- Country - Coun
T21	PRODUCT Ppt BY SOLIDS	REAGENT CONCENTRATION	1 H
T22	PRODUCT Ppt BY LIQUIDS	REAGENT CONCENTRATION	1 H
123	CONTAINMENT Ppt BY SOLIDS	REAGENT CONCENTRATION	1 H
T24	CONTAINMENT Ppt BY LIQUIDS	REAGENT CONCENTRATION	1 M
T25	SOLIDS HARVEST TANGENTIAL FLOW MF	POROSITY AVERAGE FLUX RATE TOTAL THROUGHPUT FILTRATION TIME	0.2 HICRON 11 L/SF/HR AT 40 PSIG AT 4 C 400 LITERS/SF 1 HR
126	CONTINUOUS CENTRIFUGATION SOLIDS HARVEST	SYSTEM VOID VOLUME	5 LITERS
127	7 CONTINUOUS CENTRIFUGATION SUPERNATANT HARVEST	SYSTEM VOID VOLUME	6 LITERS
12	8 DIFATION	SYSTEM VOID VOLUME	6 LITERS
12	9 BATCH CENTRIFUGATION SOLIDS HARVEST	SYSTEM VOID VOLUNE	6 LITERS

FIG. 16B

P16. 16B					
GROUP 3					
PARAMETER	SOLN.		PARAMETER	SOLN.	
Kgms of Reagent/Liters product Temperature Addition time Additional hix time		0.25 Kg/L 4 C 0.5 Hours 2 Hours	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y
LITERS REAGENT/LITERS PRODUCT TEMPERATURE ADDITION TIME ADDITIONAL MIX TIME		0.25 L/L 4 C 0.5 Hours 2 Hours	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y
Kgms of Reagent/Liters product Temperature Addition time Additional MIX time		0.25 Kg/L 4 C 0.5 Hours 2 Hours	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y
LITERS REAGENT/LITERS PRODUCT TEMPERATURE ADDITION TIME ADDITIONAL MIX TIME		0.25 L/L 4 C 0.5 Hours 2 Hours	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y Y
FLUSH PRIME CONCENTRATION FACTOR WASH REGENERATE STORE		2 L/SF 2 L/SF 10 FOLD 0.5 L/SF 1 L/SF 2 L/SF	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y Y
RCF TIME VOLUME REDUCTION WASH VOLUME		10,000 X G 60 MINUTES 30 X VOL. REDUCTION 0.2 X SYSTEM VOID VOLUME	STEP RECOVERY OF PRODUC STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y Y
RCF TIME VOLUME REDUCTION WASH VOLUME		10,000 X G 30 MINUTES 0.062 Vol. Reduction 1.5 X System Void Volume	CIP SIP		85% 0.3 Y Y Y
RCF TIME VOLUME REDUCTION WASH VOLUME		10,000 X 6 30 MINUTES 16 X YOL. REDUCTION 1.5 X SYSTEM VOID YOLUM	CIP SIP		95% 0.95 Y Y Y
RCF TIME		10,000 X 6 30 Minutes	STEP RECOVERY OF PRODU STEP RECOVERY OF T.P.	CT	95% 0.95

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FIG. 17A

	FIG. 1/A GROUP 1					
	UNIT OPERATION TYPE	PARAMETER	SOLN.	NOV 1		
	one or control of the	, meta.				
T30	BATCH CENTRIFUGATION SUPERNATANT HARVEST	SYSTEM VOID VOLUME		6 LITERS		
T31	CELL DISRUPTION HIGH PRESS. HOMOGEN.	PRODUCT TEMPERATURE UTILITY TEMPERATURE VOID VOLUME		B C 2 C 5 LITERS		
132	CELL DISPUPTION BEAD MILL	NUMBER OF PASSES BEAD SIZE VOID VOLUME FLOW RATE		2 0.5 LPM		
133	CELL DISRUPTION CHEMICAL LYSIS	REAGENT TEMPERATURE EXPOSURE TIME		0.5 M NaOH 4 C 2 HOURS		
134	MICROFILTRATION TANGENTIAL FLOW	POROSITY AVERAGE FLUX RATE TOTAL THROUGHPUT FILTRATION TIME		0.2 MICRON 50 L/SF/HR AT 40 PSIG AT 4 C 400 LITERS/SF 2 HR		
13	5 MICROFILTRATION DEAD END	POROSITY AVERAGE FLUX RATE TOTAL THROUGHPUT FILTRATION TIME		0.2 MICRON 50 L/SF/HR AT 40 PSIG AT 4 C 400 LITERS/SF 0.5 HR		
T3	G ULTRAFILTRATION CONCENTRATION/DILUTION	POROSITY AVERAGE FLUX RATE CONCENTRATION TIME		60 K NAWL 3 L/SF/HR AT 40 PSIG AT 4 C 2 HR		
T	37 ULTRAFILTRATION FLOW DIALYSIS	POROSITY AVERAGE FLUX RATE		60 K NAML 3 L/SF/HR AT 40 PSIG AT 4 C		

FIG. 17B

	GROUP 2 GROUP 3				
PARAMETER	SOLN.		PARAMETER	SOLN.	
VOLUME REDUCTION WASH VOLUME	1.5	X VOL. REDUCTION X SYSTEM VOID VOLUME	TEMPERATURE REGULATION CIP SIP	Y Y Y	
RCF TIME Volume reduction Vash volume	30	X G MINUTES X VOL. REDUCTION X SYSTEM VOID VOLUME	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	95% 0.95 Y Y Y	
NUMBER OF PASSES PRESSURE FLOW RATE TEMPERATURE INCREASE	12,000	TIMES PSI PSI PM DEGREES C/1,000 PSI	RINSE SIEP RECOVERY OF PRODUCT SIEP RECOVERY OF I.P. TEMPERATURE REGULATION CIP SIP	500% VOID VOLUMES 95% 95% Y Y Y	
-			STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	95% Y Y Y	
LITERS REAGENT/Gm PRODUCT		L/Gm HI/LITER	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	95% Y Y Y	
FLUSH PRIME WASH SOLIDS REGENERATE STORE	2.00 0.50 0.309 1.00) L/SF) L/SF) L/SF 6 OF PRODUCT SOLUTION) L/SF) L/SF	SIEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	95% 95% Y Y	
FLUSH PRIME Wash Solids Regenerate Store	0.00) L/SF) L/SF 5 L/SF 3 OF PRODUCT SOLUTION 1 L/SF 2 L/SF	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	95% 0.95 N N N	
FLUSH PRIME Wash Dilute concentrate Solids Regenerate	2.0 0.5 10. 0.30 1.0	O L/SF O L/SF O L/SF O FOLD K OF PRODUCT SOLUTION O L/SF	STORE STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	2.00 L/SF 95% 95% Y Y Y	
FLUSH PRIME DIALYSIS BUFFER WASH	2.0	2 L/SF 0 L/SF 0 X FEED STREAM VOLUKE 0 L/SF	STORE STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION	200% L/SF 95% 95% 95%	

FIG. 18A

		F16. 10	JA	ROUP 1
	UNIT OPERATION TYPE	PARAMETER	SOLN.	NOUT 1
			OOCH.	2 10
		DIALYSIS TIME		2 HR
	PROD. ADS. CHROMATOGRAPHY HPLC	COLUMN CAPACITY COLUMN OVERSIZE FACTOR COLUMN ASPECT RATIO MAX. LINEAR VELOCITY		10 Mg PROD./MI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/HR AT 45 PSIG AND 4 C
139	PROD. ADS. CHROMATOGRAPHY MPLC	COLUMN CAPACITY COLUMN OVERSIZE FACTOR COLUMN ASPECT RATIO MAX. LINEAR VELOCITY		10 Mg PROD./HI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/HR AT 45 PSIG AND 4 C
140	PROD. ADS. CHROMATOGRAPHY LPLC	COLUMN CAPACITY COLUMN OVERSIZE FACTOR COLUMN ASPECT RATIO MAX. LINEAR VELOCITY		10 Mg PROD./MI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/HR AT 45 PSIG AND 4 C
T41	CONT. ADS. CHROMATOGRAPHY HPLC	COLUMN CAPACITY COLUMN OVERSIZE FACTOR COLUMN ASPECT RATIO MAX. LINEAR VELOCITY		30 Mg CONT./MI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/H/R AT 45 PSIG AND 4 C
142	CONT. ADS. CHROMATOGRAPHY MPLC	COLUMN CAPACITY COLUMN OVERSIZE FACTOR COLUMN ASPECT RATIO MAX. LINEAR VELOCITY		10 Mg CONT./MI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/HR AT 45 PSIG AND 400% C
143	CONT. ADS. CHROMATOGRAPHY LPLC	COLUMN CAPACITY COLUMN OVERSIZE FACTOR COLUMN ASPECT RATIO MAX. LINEAR VELOCITY		10 Mg CONT./MI OF PACKING 1.5 FOLD 0.37 H/D 100 Cm/HR AT 45 PSIG AND 4 C
14	4 SIZE EXCL. CHROMATOGRAPHY HPLC	LENGTH MAX. LINEAR VELOCITY		5% OF TOTAL COLUMN VOLUME 100 Cm 100 Cm/HR AT 45 PSIG AND 4 C
14	5 SIZE EXCL. CHROMATOGRAPHY MPLC	VOID VOLUNE LOAD CAPACITY LENGTH MAX. LINEAR VELOCITY VOID VOLUNE		25% COLUMN VOLUME 5% OF TOTAL COLUMN VOLUME 100 Ca 100 Ca/Hr at 45 PSIG and 4 C 25% COLUMN VOLUME

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FIG. 18B

G	ROUP 2	P10. 10	l G	ROUP 3
PARAMETER	SOLN.		PARAMETER	SOLN.
SOLIDS REGENERATE		0.30% OF PRODUCT SOLUTION 1.00 L/SF	CIP SIP	Y. Y
COLUMN EQUILIBRATION COLUMN WASH COLUMN ELUTE A COLUMN ELUTE B COLUMN REGENERATE COLUMN STORE		5 COLUMN VOLUMES 3 COLUMN VOLUMES 3 COLUMN VOLUMES 0 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROD. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	80% 95% 95% N Y Y
COLUMN EOUILIBRATION COLUMN WASH COLUMN ELUTE A COLUMN ELUTE B COLUMN REGENERATE COLUMN STORE		5 COLUMN VOLUMES 3 COLUMN VOLUMES 3 COLUMN VOLUMES 0 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROO. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	80% 95% 95% N Y Y
COLUMN ECUILIBRATION COLUMN WASH COLUMN ELUTE A COLUMN ELUTE B COLUMN REGENERATE COLUMN STORE		5 COLUMN VOLUMES 3 COLUMN VOLUMES 3 COLUMN VOLUMES 2 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROD. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	42% 95% 95% N N Y
COLUMN EQUILIBRATION COLUMN WASH COLUMN ELUTE A COLUMN ELUTE B COLUMN REGENERATE COLUMN STORE		5 COLUMN VOLUMES 3 COLUMN VOLUMES 3 COLUMN VOLUMES 2 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES 2 COLUMN VOLUMES	PROD. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	12% 95% 95% N Y Y
COLUMN EQUILIBRATION COLUMN WASH COLUMN ELUTE A COLUMN ELUTE B COLUMN REGENERATE COLUMN STORE		5 COLUMN VOLUMES 3 COLUMN VOLUMES 3 COLUMN VOLUMES 2 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROO. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	1 42% 95% 95% N Y
COLUMN EQUILIBRATION COLUMN VASH COLUMN ELUTE A COLUMN ELUTE B COLUMN REGENERATE COLUMN STORE		5 COLUMN VOLUMES 3 COLUMN VOLUMES 3 COLUMN VOLUMES 2 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROO. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	95% N Y Y
COLUMN EQUILIBRATION COLUMN WASH COLUMN REGENERATE COLUMN STORE		4 COLUMN VOLUMES 1 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROD. ELUTION VOLUME STEP RECOVERY OF PRODUC STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	95% N Y Y
COLUMN EQUILIBRATION COLUMN WASH COLUMN REGENERATE COLUMN STORE		4 COLUMN VOLUMES 1 COLUMN VOLUMES 1 COLUMN VOLUMES 2 COLUMN VOLUMES	PROD. ELUTION VOLUME STEP RECOVERY OF PRODUC STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP	95%

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FIG. 19A

		F16. 18		
		!		GROUP 1
	UNIT OPERATION TYPE	PARAMETER	SOLN.	
146	SIZE EXCL. CHROHATOGRAPHY LPLC	LOAD CAPACITY LENGTH MAX. LINEAR VELOCITY VOID VOLUME		5% OF TOTAL COLUMN VOLUME 100 Cm/HR AT 45 PSIG AND 4 C 25% COLUMN VOLUME
T47	DILUTION	DILUTION FACTOR		3 LITERS/LITER
T48	RESOLUBILIZATION	REGEANT/PRODUCT RATIO DISSOLUTION TIME ADDITIONAL MIX TIME		0 L/Kg PRODUCT 0.50 HOURS 0.50 HOURS
TAQ	ENZYMATIC MODIFICTATON	ENZYNE TO PRODUCT RATIO		0.084 LITERS OF ENZYME STOCK PE
113	LIGHT HOUSE TELEVION	ENZYME CONCENTRATION REACTION TEMP. REACTION DURATION		LITER OF START. PROC. VOL 2 Mg/MI 37 Degrees C 30 Minutes 100%
150	LYOPHILIZATION	PRODUCT CAPACITY/LOAD PRODUCT UNIT SIZE		8 UNITS 100 GRAMS/UNIT
T51	HEAT EXCHANGE	PROCESS INITIAL TEMP PROCESS FINAL TEMP UTILITY INITIAL TEMP UTILITY FINAL TEMP PROCESS SPECIFIC HEAT DESIGN TYPE (P.T.C)		98.6 DEGREES C 39.2 DEGREES C 34 DEGREES C 5 DEGREES C 38.6 K BTU/HR P
152	STORAGE			
	FERMENTATION SEED	SCALE UP RATIO FERMENTOR WORKING VOLUME ANTIFOAM A ANTIFOAM B BASE ACID		10 FOLD 50 LITERS 1 HI/L 1 HI/L 5 HI/L 5 HI/L
15	4 INITIAL SEEDING	FLASK FEED VOLUME SPINNER SPLIT RATIO		12 LITERS

FIG. 19B

	ROUP 2		<i>F16.</i> 1	30	30UP 3	
PARAMETER	SOLN.			PARAMETER	SOLN.	
COLUMN EQUILIBRATION COLUMN WASH COLUMN REGENERATE COLUMN STORE		1 1 2	COLUMN VOLUMES COLUMN VOLUMES COLUMN VOLUMES COLUMN VOLUMES	PROD. ELUTION VOLUME STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		42% COLUMN VOLUMES 95% 95% N Y
DILUTION TIME ADDITIONAL MIX TIME			HOURS HOURS	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y Y
REGEANT 1 Concentration		WATER DIST.		STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y Y
TITRATION SOLUTION-1 TITRATION SOLUTION-2 NEUTRALIZATION		0.02	L/L PROCESS L/L PROCESS L/L PROCESS	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% 95% Y Y Y
LYOPHILIZATION TIME PRODUCT WEIGHT REDUCTION		18 0.95	HOURS	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. CIP SIP		95% 95% Y Y Y
EXPOSURE TIME		1	L HOURS	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP STEP RECOVERY OF PRODUC		100% 100% Y Y Y Y
				STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		95% Y Y Y
GROWTH TEMPERATURE AGITATION SPARGE RATE BACK PRESSURE TOTAL DURATION		1.	17 HOURS 1 HP/100L 5 VVH 5 PSIG 11 HRS	FINAL OD CIP		12 Y
SERUM CONTENT FEED RATE		2	% FBS 1 FEED PER VESSEL PE	AMPLIFICATION FACTOR		1

FIG. 20A

			6	ROUP 1
	UNIT OPERATION TYPE	PARAMETER	SOLN.	
		UCARRIER DENSITY NUMBER OF PBS VASHES NUMBER OF MEDIA VASHES NO. OF MEDIA/SERUM VASHES		5 Gm/LITER 2 1 2 FBS
T55	CULTURE VESSEL SPLIT	FLASK FEED VOLUME		12 LITERS
		SPINNER SPLIT RATIO UCARRIER DENSITY NUMBER OF PBS WASHES NUMBER OF MEDIA WASHES NO. OF MEDIA/SERUM WASHES		4 5 Gm/LITER 2 1 2 FBS
-	CULTURE FLASK SPLIT			
157	STIRRED TANK REACTOR			
158	FLUIDIZED BED REACTOR	PROCESS INITIAL TEMP PROCESS FINAL TEMP UTILITY INITIAL TEMP UTILITY FINAL TEMP PROCESS SPECIFIC HEAT DESIGN TYPE (P.T.C)		37 DEGREES C 4 DEGREES C 2 DEGREES C 5 DEGREES C 12 K BTU/HR P
159	LIQUID/LIQUID EXTRACTION	LIQUID/LIQUID RATIO EXTRACTION TEMPERATURE ADDITION DURATION ADDITIONAL MIX. DURATION MIX ENERGY		1 L EXTRACTION/L PRODUCT 4 C 0.5 Hours 4 Hours 0.3 HP/100L
T60	SOLID/LIQUID EXTRACTION	LIQUID/LIQUID RATIO EXTRACTION TEMPERATURE DURATION MIX ENERGY		1 L EXTRACTION/L PRODUCT 4 C 4 HOURS 0.3 HP/100 L

FIG. 20B

	GROUP 2		G	ROUP 3	
Parameter	SOLN.		PARAMETER	SOLN.	
DAYS TO CONFLUENCE		2 DAYS 2 DAYS			
SERUM CONTENT		2% FBS	AMPLIFICATION FACTOR		1
FEED RATE		1 FEED PER VESSEL PER			
DAYS TO CONFLUENCE		2 DAYS 2 Days			,
EXPOSURE TIME		50% HOURS	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. CIP SIP STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P.		0.95 95% Y Y Y 0.95
			TEMPERATURE REGULATION CIP		Y Y Y Y
PHASE SEPARATION TIME PRODUCT PHASE (TOP/BOTTOM) HARVEST TIME		1600% HOURS TOP 0.5 HOURS	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		0.9 50% Y Y Y
PHASE SEPARATION TIME PRODUCT PHASE (TOP/BOTTOM) HARVEST TIME		1600% HOURS TOP 0.5 HOURS	STEP RECOVERY OF PRODUCT STEP RECOVERY OF T.P. TEMPERATURE REGULATION CIP SIP		0.9 50% Y Y Y

			P.	Process Design Cycles	sign (Sycles						
QOD		•	Ľ.	Unit Op		Unit	Unit Op Cluster	5	<u></u>		Batch	
Seq.	No. Code	Unit Operation Type		Offset (Hrs)		UnOp Start	UnOp End	Offset (Hrs)		UnOp Start	UnOp End	Offset (Hrs)
	89	STR-Suspension Production	_	0				0	_			0
2	74	Harvest/Feed-Suspension Production	က	24				0	20	2	4	72
3	34	Tangential Flow-Clarification	_	0	—			0	70	2	4	72
4	47	Dilution	_	0				0	20	7	4	72
ည	66	End				-						
2102 2104	104	2106 2108		2108 2110 2112 2114	12 2		2116	2118 2120 2122			2124	2126

FIG. 2

			Po	Process Design Cycles	n Cycles						
				Unit Op	5	Unit Op Cluster	ter			Batch	
Seq.	Seq. No. Code	Unit Operation Type		Offset (Hrs)	UnOp Start	ChOp	Offset (Hrs)		UnOp Start	ChO Prad	Offset (Hrs)
10301	87	Pool	_				·				
10302	51	Heat Exchange	_	<u> </u>				-			
10303	97	Cont. Centrifugation - Solids Harvest	-	· <u> </u>	<u>.</u>			_			
10304	84	Resolubilization	_	-				_			
10305	61	Inlet Heat Exchange	_		3	7		-			
10306	31	High Pressure Homogenization			3	7	Ø	_			
10307	51	Outlet Heat Exchange	_		3		Ø				
10308	53	Batch Centrifugation - Solids Harvest	-								
10309	53	Dilution - IB Wash			2 9			4			
10310	53	Batch Centrifugation - Solids Harvest	-		2 9	9					
10311	63	Storage	~-	· ·							
10312	66	End		•				_			
2202 2204	04	2208	_	2210 2212	2214	2216	2218 2220	2222		2224	2226

FIG. 22

·			· · · · · · · · · · · · · · · · · · ·			
	OPERATION		CALC	CULATIONS		
1.1.1.1 176	MUTI-STAGE POOL	LINK Source				
	SET_UP					
	INPUT 1 INPUT 2	PE-0102e	20272.98 LITERS 0 0 LITERS 0	104.00 Hours, Transfer in 0.00 Hours, Transfer in	0.0 Hours= 0.0 Hours=	0.0 LP 0.0 LP
	INPUT 3		O LITERS O	0.00 Hours transfer in	0.0 HOURS=	0.0 LP
	INPUT 4 INPUT 5		0 Liters 0 0 Liters 0	0.00 Hours, transfer in 0.00 Hours, transfer in	0.0 Hours= 0.0 Hours=	0.0 LP 0.0 LP
	INPUT 6		O LITERS 😉	0.00 HOURS, TRANSFER IN	0.0 HOURS=	0.0 LP
	POOL INPUTS		20272.98 LITERS IN	0.00 Hours, transfer in	0.0 Hours=	0.0 LP
	SUB TOTAL			104.00 TOTAL TRANSFER	0 HOURS	LPM MISC
2.1.1.1 51	OUTLET HEAT EXCHANGE				,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	
	SET UP	20.277.0 1 10	a ca une	176 0 100		
	Transfer Wash	20,273.0 L IN	2.50 HRS =	135.2 LPM		
	CIP					
	SIP CLEAN UP					
	SUB TOTAL			135.2		
3111 26	CONT. CERT/SOLIDS				-	
J.1.1.1 20	SET UP					
	CENTRIFUGATION	20,273.0 L IN	5.00 HRS =	56.3 LPM		
	WASH CIP	30.0 L IN	0.01 HRS =	56.3 LPM		
	SIP					
	CLEAN UP			F6.7 1001	<u></u> -	
	SUB TOTAL			56.3 LPM		
4.1.1.1 48	RESOLUBILIZATION					
	SET UP	6.136.0.1.111	3.0.1101/00	70.6 (0)		
	DILUTION NO	6,476.0 L IN	3.0 Hours 0.0 Hours	38.0 LPM		
	CIP		0.0 1100113			
	SIP CLEAN UP					
	SUB TOTAL			36.0		
				•		
5.1.1.1 61	INLET HEAT EXCHANGE					
	set up Transfer	8,634.7 L IN	2.5 HRS =	57.56 LPM		
	WASH ,	0.0 L IN	2.5 HRS = 0.0 HRS =	0.0 LPM		
	7					
	2302			2304		

FIG.23A-1

			IV.L. III	E SCALE	(cuu)	ABS. H	JUKS	ABS. D	112	START		FINISH	
CALC.	ΓOC	ADJ.	PREP	EXEC.	COMPL.	START	END	START	END	DATE	TIME	DATE	TIME
0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	104.0	104.0		104.0 104.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0	104.0 104.0 0.0 0.0 0.0 0.0 0.0 0.0 0.0 104.0	4.33 4.33 0.00 0.00 0.00 0.00 0.00 0.00	4.33 4.33 0.00 0.00 0.00 0.00 0.00 0.00	01/08/99 01/08/99 01/08/99	06:00 AM 06:00 AM	01/08/99 01/08/99 01/08/99	08:00 AM
0.0	0.0	0.0 HRS		104.0		104.0	0.0	7.33		01/08/99 HRS/CY OK	06:00 AM 06:00 AM 0.0		08:00 AM 08:00 AM
1.0 2.50 0.63 0.0 0.0 2.0	0.0 0.0 0.0	1.0 HRS 2.5 HRS 0.5 HRS 0.0 HRS 0.0 HRS 2.0 HRS	104.0	106.5 107.1	107.1 107.1 109.1	103.0 104.0 106.5 107.1 107.1	104.0 105.5 107.1 107.1 107.1 109.1	4.28 4.33 4.44 4.46 4.46 4.46	4.33 4.44 4.46 4.46 4.46 4.55	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	07:00 AM 08:00 AM 10:30 AM 11:07 AM 11:07 AM	01/08/99 01/08/99 01/08/99	08:00 AM 10:30 AM 11:07 AM 11:07 AM 11:07 AM 01:07 PM
5.1		5.1 HRS		106.5						01/08/99 HRS/CY OK	07:00 AM 5.1		01:07 PM
1.0 6.0 0.0 0.0 0.0	0.0 0.0 0.0	1.0 HRS 6.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	105.6	112.5 112.5	112.5 112.5 112.5	105.6 106.5 112.5 112.5 112.5 112.5	106.5 112.5 112.5 112.5 112.5 112.5	4.00 4.64 4.68 4.68 4.68 4.68	4.44 4.64 4.68 4.68 4.68 4.68	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	09:30 AM 10:30 AM 04:10 PM 04:10 PM 04:30 PM 04:30 PM	01/08/99	10:30 AW 04:30 PW 04:30 PW 04:30 PW 04:30 PW 04:30 PW
7.0		7.0 HRS		112.5			112.5			01/08/99 HRS/CY OK	09:30 AM 3.0		04:30 PM
1.0 3.00 0.00 0.0 0.00 1.00	0.0 0.0 0.0 0.0	1.0 HRS 3.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS 1.0 HRS		115.5 115.5	115.5 115.5 116.5	111.0 112.5 115.5 115.5 115.5	112.0 115.5 115.5 115.5 115.5 118.5	4.85 4.88 4.81 4.81 4.81 4.81	4.68 4.81 4.81 4.81 4.81 4.85	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	03:30 PM 04:30 PM 07:30 PM 07:30 PM 07:30 PM 07:30 PM	01/08/99 01/08/99 01/08/99	04:30 PM 07:30 PM 07:30 PM 07:30 PM 07:30 PM 08:30 PM
5.00		5.00 HRS		115.5						01/08/99 HRS/CY OK		01/08/99	08:30 PM
1.0 2.50 0.00	0.0	1.0 HRS 2.5 HRS 0.0 HRS		118.0 118.0		114.5 115.5 118.0	118.0	4.81	4.81 4.92	01/08/99 01/08/99 01/08/99	07:30 PM	01/08/99 01/08/99 01/08/99	07:30 PN 10:00 PN 10:00 PN

	OPERATION			CA	CULATIONS	
	CIP SIP					
	CLEAN UP					
	SUB TOTAL				57.6	
6.1.1.1 31	HOMMOCENIZATION					····
	SET UP LYCIS	70747 I III	3.5.1100		63.6 LDU	
	WASH	3834.7 L IN 0.0 L IN		= =	57.6 LPM 0.0 LPM	
	CIP				575 64	
	SIP CLEAN UP					
	SUB TOTAL		······	5	7.564344	
7111 51	OUTLET HEAT EXCHANGE					
1.1.1.1 JI	SET UP					
	TRANSFER	3543.7 L IN	2.5 HRS	=	57.58 LPM	
	WASH CIP	0.0 L IN		=	0.0 LPM	
	SIP					
	CLEAN UP					
	SUB TOTAL				57.56	
5.1.2.1 61	INLET HEAT EXCHANGE					
	SET UP	00747.4 111	25.422			
	Transfer Wash	8634.7 L IN 0.0 L IN		=	57.56 LPM 0.0 LPM	
	CIP	0.0 (0.0 TM3	_	0.0 CI M	
	SIP CLEAN UP					
	SUB TOTAL					
<u> </u>	110111100051117171011	···				
b.1.Z.1 31	HOMMOGENIZATION					
	SET UP DILUTION	6834.7 L IN	2.5 HRS	=	57.6 LPM	
	MO I	0.0 L IN		=	0.0 LPM	
	CIP					
	SIP CLEAN UP					
	SUB TOTAL				57.56	

FIG.23B-1

DURATION	(HRS)		REL. TIN	E SCALE	(HRS)	ABS. H	OURS	ABS. D	AYS	START		FINISH	
CALC.	Γ0C	ADJ.	PREP	EXEC.	COMPL.	START	END	START	END	DATE	TIME	DATE	TO
0.0 0.0 0.0	0.0 0.0 0.0	0.0 HRS 0.0 HRS 0.0 HRS			118.0 118.0 118.0	118.0 118.0 118.0	118.0 118.0 118.0	4.92 4.92 4.92	4.92 4.92 4.92	01/08/99 01/08/99 01/08/99	10:00 PM 10:00 PM 10:00 PM	01/08/99 01/08/99 01/08/99	10:00 I 10:00 I 10:00 I
2.5		2.5 HRS		116.0						01/08/99 HRS/CY OK	06:30 PM 3.5	01/08/99	10:00
1.0 2.5 0.00 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0	1.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	118.0	120.5 120.5	120.5 120.5 120.5	117.0 118.0 120.5 120.5 120.5 120.5	118.0 120.5 120.5 120.5 120.5 120.5	4.88 4.92 5.02 5.02 5.02 5.02	4.92 5.02 5.02 5.02 5.02 5.02	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 10:00 PM 12:30 AM 12:30 AM 12:30 AM	01/08/99 01/08/99 01/08/99 01/08/99	10:00 1 12:30 1 12:30 1 12:30 1 12:30 1
3.5		3.5 HRS		120.5			120.5			01/08/99 HRS/CY OK	09:00 PM 3.5		12:30
1.0 2.50 0.00 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0	1.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	120.5	123.0 123.0	123.0 123.0 123.0	118.5 120.5 123.0 123.0 123.0 123.0	120.0 123.0 123.0 123.0 123.0 123.0	4.88 5.02 5.13 5.13 5.13 5.13	5.02 5.13 5.13 5.13 5.13 5.13	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	11:30 PM 12:30 AM 03:00 AM 03:00 AM 03:00 AM	01/08/99 01/08/99 01/08/99	12:30 03:00 03:00 03:00 03:00
2.5		2.5 HRS		123.0						01/08/99 HRS/CY OK	11:30 PM 3,5		03:00
0.0 2.50 0.00 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	123.0	125.5 125.5	125.5 125.5 125.5	123.0 123.0 125.5 125.5 125.5 125.5	123.0 125.5 125.5 125.5 125.5 125.5	5.13 5.13 5.23 5.23 5.23 5.23	5.13 5.23 5.23 5.23 5.23	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	05:30 AM		03:00 05:30 05:30 05:30 05:30 05:30
2.5		2.5 HRS		125.5 Q1F895						01/08/99 HRS/CY OK	03:00 AM 2.5	01/08/99	05:30
1.0 2.5 0.00 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	123.0	125.5 125.5	125.5 125.5 125.5	123.0 123.0 125.5 125.5 125.5 125.5	123.0 125.5 125.5 125.5 125.5 125.5	5.13 5.13 5.23 5.23 5.23 5.23	5.13 5.23 5.23 5.23 5.23 5.23		03:00 AM 03:00 AM 05:30 AM 05:30 AM 05:30 AM	01/08/99 01/08/99	03:00 05:30 05:30 05:30 05:30
2.5		2.5 HRS		125.5			125.5			01/08/99 HRS/CY OK		01/08/99	05:30

FIG.23B-2

		*				
·	OPERATION			CAL	CULATIONS	
TR W/ Ci Si Ci	T UP CANSFER ASH P P EAN UP JB TOTAL	8543.7 L IN 0.0 L IN	2.5 HRS 0.0 HRS	= =	57.56 LPH 0.0 LPH	
SE Th W. Ci Si Ci	LET HEAT EXCHANGE T UP VANSFER ASH P P LEAN UP JB TOTAL	8634.7 L IN 9.0 L IN		= =	57.58 LPM 57.6 LPM	
CI SI SI SI	DMMOCENIZATION ET UP CIS ASH P P LEAN UP JB TOTAL	8634.7 L IN 9.0 L IN	2.5 HRS 0.0 HRS	= =	57.6 LPM 57.6 LPM 57.56 LPM	
SI TF W CI SI CI		8643.7 L IN 9.0 L IN	2.5 HRS 0.0 HRS	=======================================	57.50 LPM 57.6 LPM	

FIG.23C-1

CALC.	ιœ		1100. 1101	E SCALE	(unz)	ABS. HO	UKS	ABS. DA	113	START		FINISH	
0.0	- 100	ADJ.	PREP	EXEC.	COMPL.	START	END	Start	END	DATE	TIME	DATE	Ţ
2.50 0.00 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	123.0	125.5 125.5	125.5 125.5 125.5	123.0 123.0 125.5 125.5 125.5 125.5 125.5	123.0 125.5 125.5 125.5 125.5 125.5	5.13 5.13 5.23 5.23 5.23 5.23	5.13 5.23 5.23 5.23 5.23 5.23 5.23	01/08/99 01/08/99 01/08/99 01/08/99	05:30 AM 05:30 AM 05:30 AM 05:30 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	03:00 05:30 05:30 05:30 05:30 05:30
2.5		2.5 HRS		125.5						01/08/99 HRS/CY OK	03:00 AM 2.5	01/08/99	05:30
0.0 2.50 0.0 0.0 0.0	0.0 0.0 0.0 0.0 0.0 0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS	125.5	128.0 128.0	128.0 128.0 128.0	125.5 125.5 128.0 128.0 128.0 128.0	125.5 128.0 128.0 128.0 128.0 128.0	5.23 5.33 5.33 5.33 5.33 5.33	5.23 5.33 5.33 5.33 5.33 5.33	01/08/99 01/08/99 01/08/99 01/08/99	05:30 AM 05:30 AM 08:00 AM 08:01 AM 08:01 AM 08:01 AM	01/08/99 01/08/99 01/08/99	05:30 08:00 08:01 08:01 08:01 08:01
2.5		2.5 HRS		128.0						01/08/99 HRS/CY OK	05:30 AM 2.5	01/08/99	08:01
0.0 2.5 0.0 0.0 0.0	0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS		128.0 128.0	128.0 128.0 128.0	125.5 125.5 128.0 128.0 128.0 128.0	125.5 128.0 128.0 128.0 128.0 128.0	5.23 5.23 5.33 5.33 5.33 5.33	5.23 5.33 5.33 5.33 5.33 5.33	01/08/99 01/08/99 01/08/99 01/08/99	05:30 AM 05:30 AM 08:00 AM 08:01 AM 08:01 AM 08:01 AM	01/08/99 01/08/99 01/08/99 01/08/99	05:30 08:00 08:01 08:01 08:01 08:01
2.5		2.5 HRS		128.0			128.0			01/08/99 HRS/CY * OK	05:30 AM 2.5	01/08/99	08:01
0.0 2.50 0.0 0.0 0.0	0.0 0.0 0.0 0.0	0.0 HRS 2.5 HRS 0.0 HRS 0.0 HRS 0.0 HRS 0.0 HRS		128.0 128.0		128.0	125.5 128.0 128.0 128.0 128.0 128.0	5.23 5.33 5.33 5.33	5.33 5.33 5.33 5.33	01/08/99 01/08/99 01/08/99 01/08/99	05:30 AM 05:30 AM 08:01 AM 08:01 AM 08:01 AM	01/08/99 01/08/99 01/08/99 01/08/99	05:30 08:01 08:01 08:01 08:01 08:01

FIG.23C-2

		first shift				SECOND SH	IFT		
	;	START	07:00 AM	FINISH	03:00 PM	START	03:00 PM	FINISH	11:00 PY
	OPERATION	DATE	TIME	DATE	TIME	DATE	TIME	DATE	TIME
	MUTI-STAGE POOL SET UP INPUT 1 INPUT 2 INPUT 3 INPUT 4	01/08/99 01/08/99	08:00 AM 08:00 AM	01/08/99 01/08/99	08:00 AM 08:00 AM				
	INPUT 5 INPUT 6 POOL INPUTS SUB TOTAL	01/08/99	MA 00:80	01/08/99	08:00 AM				
2.1.1.1 51	OUTLET HEAT EXCHANCE SET UP TRANSFER WASH CIP SIP CLEAN UP SUB TOTAL	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 10:30 AM 11:07 AM 11:07 AM		08:00 AM 10:30 AM 11:07 AM 11:07 AM 11:07 AM 01:07 PM				
3.1.1.1 26	CONT. CERT/SOLIDS SET UP CENTRIFUCATION WASH CIP SIP CLEAN UP SUB TOTAL	01/08/99 01/08/99	09:30 AM 10:30 AM		10:30 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	04:30 PM 04:30 PM 04:30 PM 04:30 PM 04:30 PM		04:30 PM 04:30 PM 04:30 PM 04:30 PM 04:30 PM
4.1.1.1 48	RESOLUBILIZATION SET UP DILUTION MO CIP SIP CLEAN UP SUB TOTAL					01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	03:30 PM 04:30 PM 07:30 PM 07:30 PM 07:30 PM 07:30 PM	01/08/99 01/08/99 01/08/99 01/08/99	04:30 PW 07:30 PW 07:30 PW 07:30 PW 07:30 PW
5.1.1.1 61	INLET HEAT EXCHANCE SET UP TRANSFER WASH					01/08/99 01/08/99 01/08/99	07:30 PM	01/08/99 01/08/99 01/08/99	10:00 Pk

FIG.23D-1

third shif	1		
START	11:04 PM	FINISH	04:07 AM
DATE	TIME	DATE	TIME
01/08/99	07:00 AM		

FIG.23D-2

	FIRST SHIFT			second shift				
	START	07:00 AM	FINISH	03:00 PM	START	01:00 PM	FINISH	11:00 PM
OPERATION	DATE	TIME	DATE	TIME	DATE	TIME	DATE	TIME
CIP SIP CLEAN UP SUB TOTAL					01/08/99 01/08/99 01/08/99	10:00 PM 10:00 PM 10:00 PM	01/08/99 01/08/99 01/08/99	10:00 PM 10:00 PM 10:00 PM
6.1.1.1 31 HOMMOGENIZATION SET UP LYCIS WASH CIP SIP CLEAN UP SUB TOTAL					01/08/99 01/08/99	09:00 PM 10:00 PM	01/08/99	10:00 PM
7.1.1.1 51 OUTLET HEAT EXCHANCE SET UP TRANSFER WASH CIP SIP CLEAN UP SUB TOTAL								
5.1.2.1 61 INLET HEAT EXCHANGE SET UP TRANSFER WASH CIP SIP CLEAN UP SUB TOTAL								
6.1.2.1 31 HOMMOCENIZATION SET UP LYCIS WASH CIP SIP CLEAN UP SUB TOTAL								

FIG.23E-1

START	11:00 PM	FINISH	08:00 AM		
DATE	TIME	DATE	TIME		
v					
		-			
		01/08/99	12:30 AW		
01/08/99	12:30 AM	01/08/99	12:30 AV		
01/08/99	12:30 AM	01/08/99	12:30 AM		
01/08/99 01/08/99	11:30 PM 12:30 AM	01/08/99 01/08/99	12:30 AM 03:00 AM		
01/08/99	03:00 AM 03:00 AM	01/08/99	03:00 AW 03:00 AW		
01/08/99 01/08/99	03:00 AM 03:00 AM	01/08/99 01/08/99	03:00 AW 03:00 AW		
01/08/99	03:00 AM	01/08/99	03:00 AV		
01/08/99 01/08/99	03:00 AM 05:30 AM	01/08/99 01/08/99	05:30 AN 05:30 AN		
01/08/99	05:30 AM 05:30 AM	01/08/99	05:30 AM 05:30 AM		
01/08/99	05:30 AM	01/08/99	05:30 AX		
01/08/99	03:00 AM	01/08/99	03:00 AJ		
01/08/99 01/08/99	03:00 AM 05:30 AM	01/08/99	05:30 AA 05:30 AA		
01/08/99 01/08/99	05:30 AM 05:30 AM	01/08/99	05:30 AA 05:30 AA		
01/08/99	05:30 AM		05:30 A		

FIG.23E-2

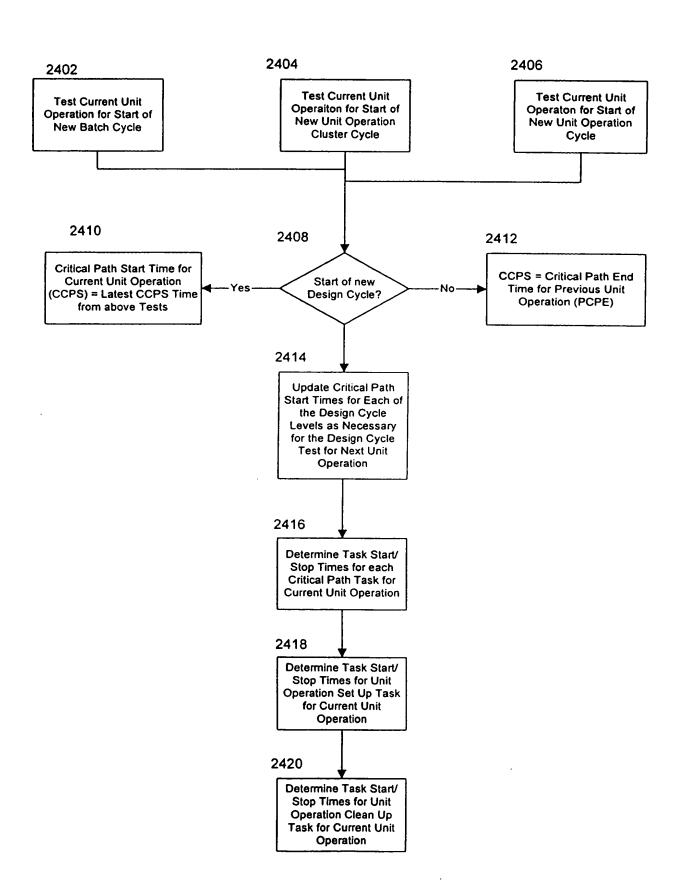
		first shift				SECOND S	HIFT		
	-	START	07:00 AM	FINISH	03:00 PM	START	03:00 PM	FINISH	11:00 PM
	OPERATION	DATE	TIME	DATE	TIME	DATE	TIME	DATE	TIME
	SET UP TRANSFER WASH CIP SIP CLEAN UP SUB TOTAL								
5.1.3.1 61	INLET HEAT EXCHANGE SET UP TRANSFER WASH CIP SIP CLEAN UP SUB TOTAL	01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 08:01 AM 08:01 AM 08:01 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 08:01 AM 08:01 AM 08:01 AM 08:01 AM				
6.1.3.1 31	HOMMOGENIZATION SET UP LYCIS WASH CIP SIP CLEAN UP SUB TOTAL	01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 08:01 AM 08:01 AM	01/08/99 01/08/99 01/08/99 01/08/99 01/08/99	08:00 AM 08:01 AM 08:01 AM 08:01 AM				
7.1.3.1 51	OUTLET HEAT EXCHANGE SET UP TRANSFER WASH CIP SIP CLEAN UP SUB TOTAL	01/08/99 01/08/99 01/08/99 01/08/99	08:01 AM 08:01 AM 08:01 AM 08:01 AM	01/08/99 01/08/99	08:01 AM 08:01 AM 08:01 AM 08:01 AM				

FIG.23F-1

THIRD SHIFT	······································		
START	11:00 PM	FINISH	05:30 AM
DATE	TIME	DATE	TIME
01/08/99 01/08/99	03:00 AM 03:00 AM	01/08/99 01/08/99	03:00 AM 05:30 AM
01/08/99	05:30 AM 05:30 AM	01/08/99	05:30 AM 05:30 AM
01/08/99 01/08/99	05:30 AM 05:30 AM	01/08/99 01/08/99	05:30 AM 05:30 AM
01/00/33	UU:JU AM	01/00/33	UJ.JU AM
01/08/99 01/08/99	05:30 AM 05:30 AM	01/08/99	05:30 AM
			:
01/08/99	05:30 AM	01/08/99	05:30 AM
01/08/99	05:30 AM		
01 (00 (00	05.70.411	01 (00 (00	05:30 AM
01/08/99 01/08/99	05:30 AM 05:30 AM		UD:3U AM

FIG.23F-2

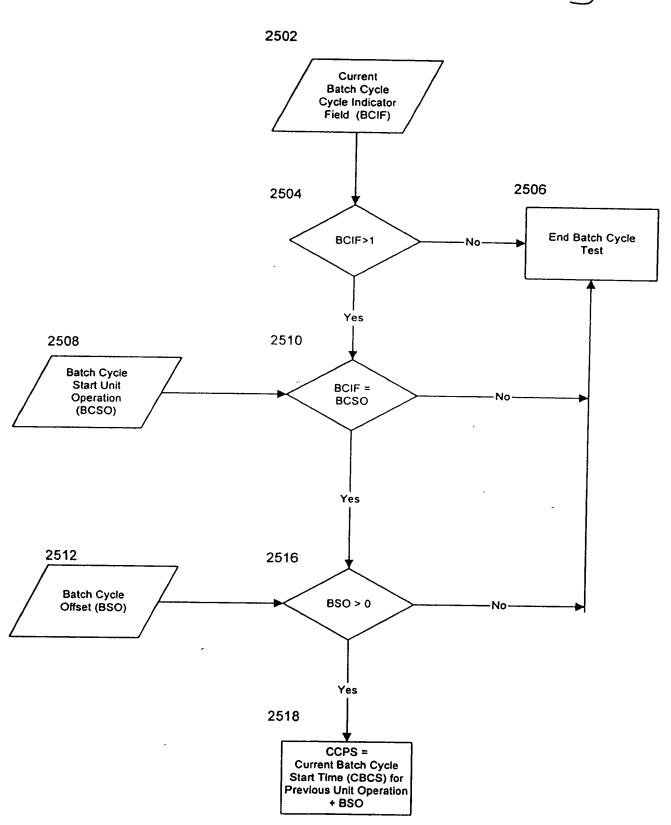
FIG. 24

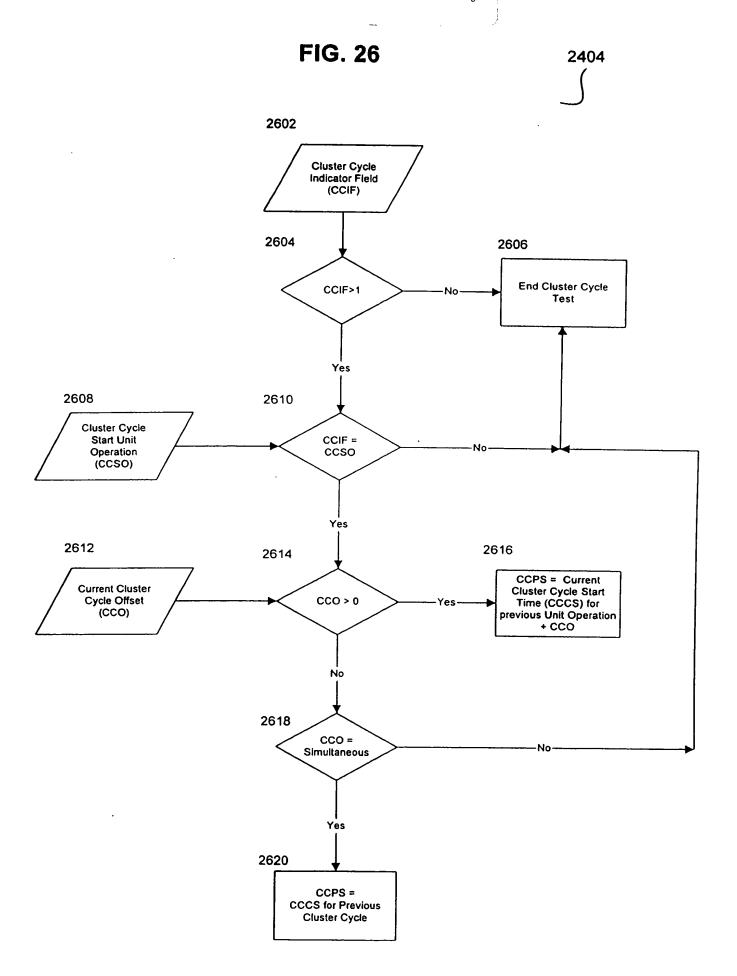


Appl. No. To Be Assigned; Filed: HEREWITH Dkt. No. 1606.0010003; Group Art Unit: TBA Inventor(s): Peter G. BROWN; Tel: 202/371-2600

Title: System And Method For Simulation And Modeling...









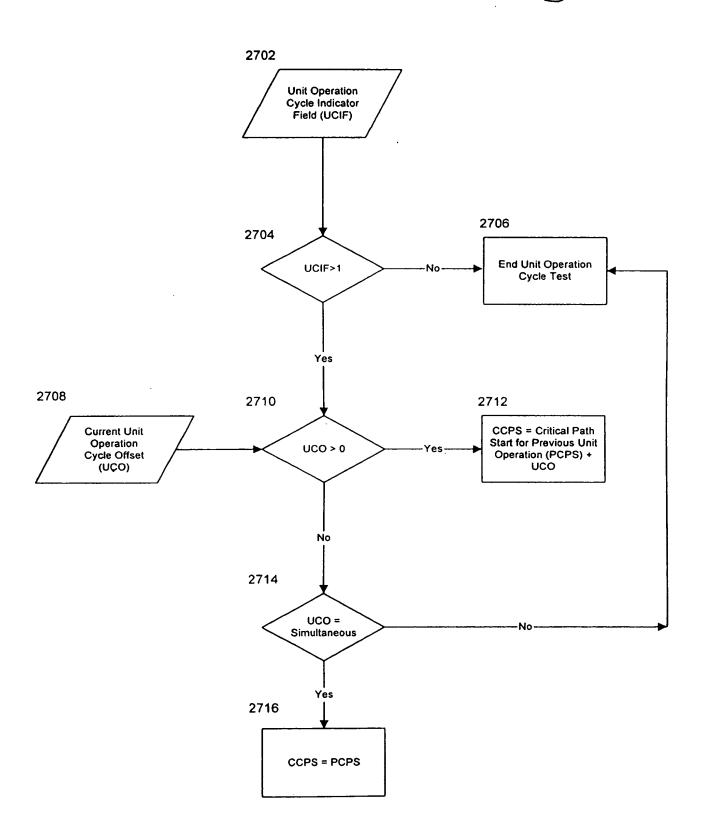


FIG. 28

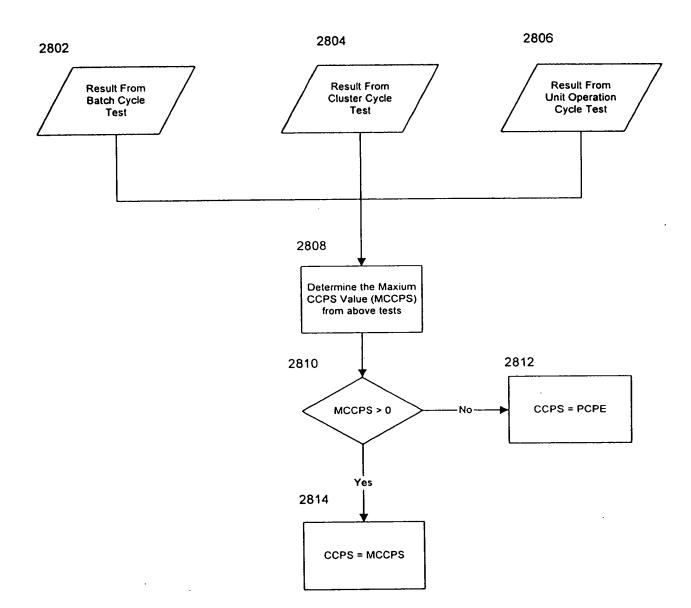


FIG. 29

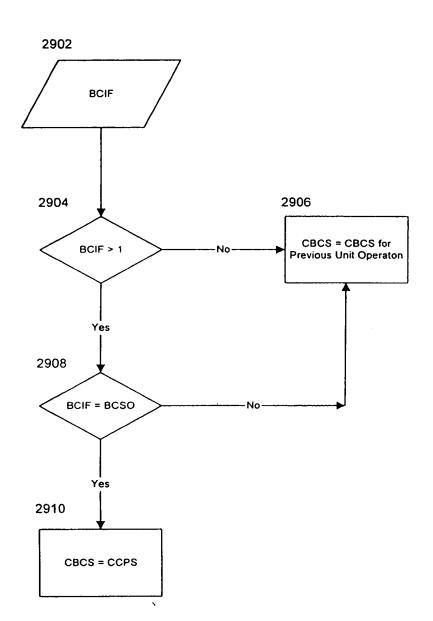


FIG. 30

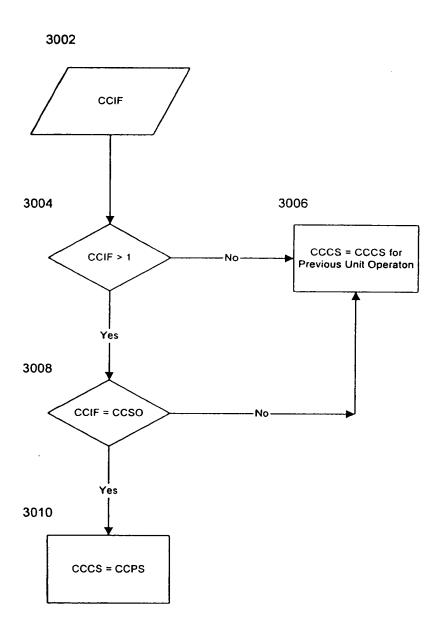


FIG. 31

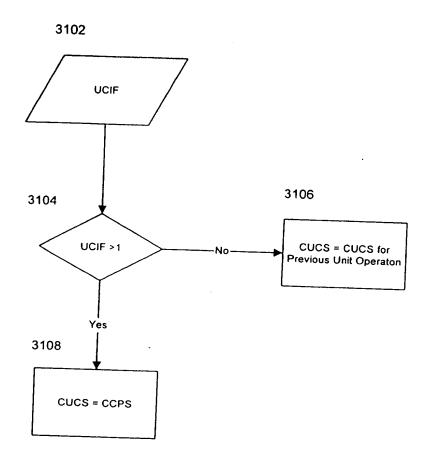


FIG. 32

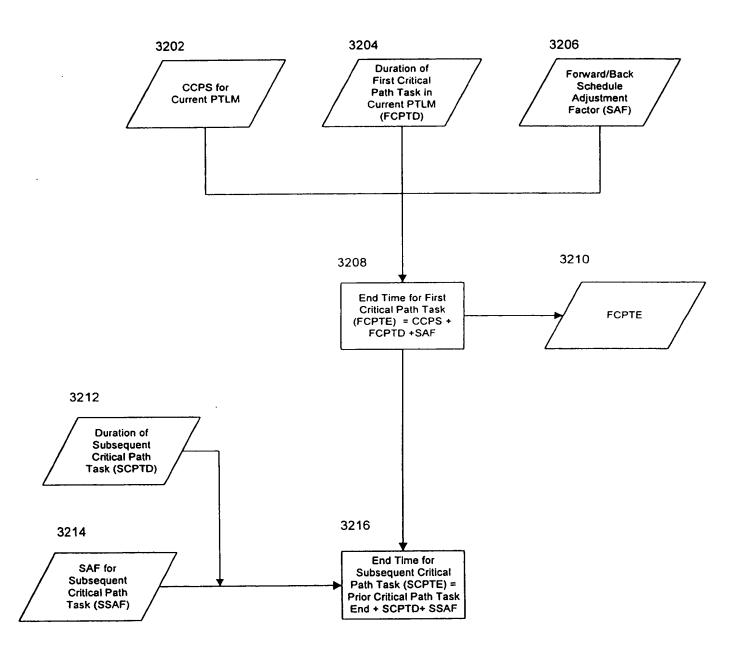


FIG. 33

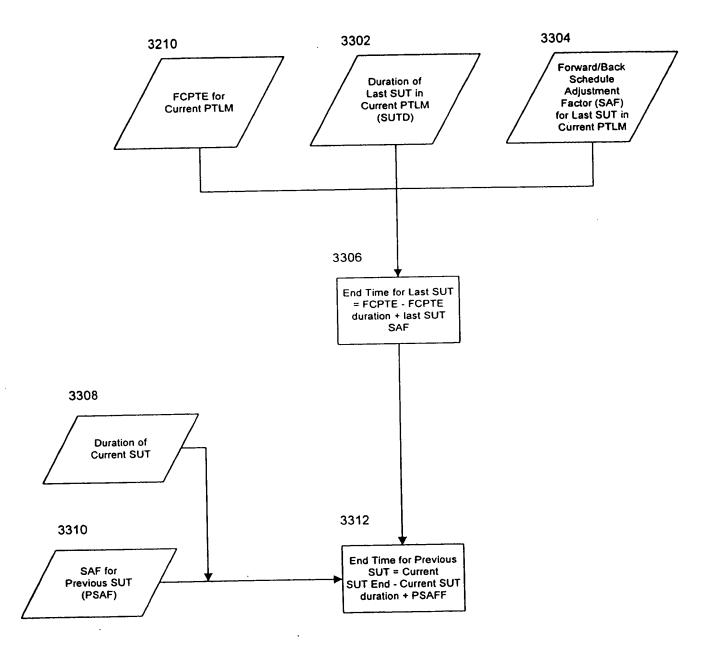


FIG. 34

